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Numerical Simulation of Fluid Dynamics and Combustion for Ram Accelerator Projectile/Obturator Interaction

Michael J. Nusca

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1. INTRODUCTION

Numerical simulation of the ram accelerator has been an ongoing research project at the U.S. Army Research Laboratory (ARL) since 1990 (Nusca 1990, 1991, 1992). Computational fluid dynamics solutions of the Navier-Stokes equations have been applied to turbulent non-reacting and reacting in-bore flowfields for a ram accelerator projectile launch system. Numerical simulations reveal in-bore flowfield details and provide comparison with measured launch tube wall pressures and projectile thrust as a function of velocity. Numerical simulations are also used to investigate the ARL 120mm (bore diameter) ram accelerator system. These simulations are used as a system design aid and as a means by which geometric and fluid dynamic scaling phenomena are investigated.

For non-reacting flow simulations the Rockwell Science Center USA-PG (Unified Solution Algorithm Perfect Gas) code is used (Chakravarthy 1985,1989). In this code the Navier-Stokes equations are cast in conservation form and converted to algebraic equations using upwind and central finite differences and finite-volume formulations. The equations are solved using a second-order TVD (total variation diminishing) scheme. The code is capable of simulating mixed subsonic/supersonic flowfields.

For finite-rate reacting flow simulations the ARL-RAMCOMB (RAMjet COMBustion) code (Nusca, May 1990) has been used. The steady 2D/axisymmetric Navier-Stokes equations are written in stream function-vorticity form and solved using a Gauss-Seidel relaxation scheme. These equations include conservation of chemical species and reacting flow source terms in the energy equation. Both one-step/global and three-step finite-rate reaction mechanisms for fuel (CH_4) and oxidizer (O_2) are considered. In addition, the latest versions of the USA-series codes are being utilized (Ota 1988, Palaniswamy 1989). These codes include both equilibrium (USA-EC) and finite-rate (USA-RG) chemistry which is fully coupled to the gasdynamics and are capable of time-accurate simulations. Comparison of results from the USA-RG and RAMCOMB codes will be reported as well as comparisons between the USA-EC code and finite-rate computations.

Results for the ram accelerator projectile excluding the obturator have been published (Nusca 1990,1991,1992). These numerical simulations used non-reacting or reacting flow codes (in the case of the reacting flow previous efforts used a coupling procedure for the USA-PG and ARL-RAMCOMB codes) to simulate the effects of acceleration on the projectile flowfield. Numerical simulations provided a possible explanation of the thrust/velocity curve as well as data on the fluid dynamic and reacting flow scaling effects. These results are not repeated in the present report and the reader is referred to Nusca (Nov. 1991) for details. It is the purpose of the present report to investigate the projectile/obturator separation

and combustion starting process using non-reacting flow codes (USA-PG) as well as a fully coupled finite-rate chemistry code (USA-RG). Whereas previous simulations have been for steady and quasi-steady flows, the present report focuses on time-accurate predictions of time-dependent flow phenomena.

The ram accelerator projectile geometry used in these studies represents a simplification of the actual configuration used for test firings. The actual projectile includes a set of four bore-riding fins that extend from the point of maximum projectile diameter to the projectile base and span the area between the projectile and the launch tube. Exclusion of these fins permits a 2D/axisymmetric calculation and results in a significant computer time savings over the full 3D numerical simulation. Such 3D simulations have been performed with the present codes.

2. BACKGROUND

The ram accelerator technique was first investigated via experimental test firings at the University of Washington (UW) (Hertzberg 1988, Bruckner 1988/1991, Knowlen 1992). The UW ram accelerator facility uses a light gas gun (e.g. helium driver gas) to accelerate projectiles up to 1300 m/s. The muzzle is connected to a perforated tube and evacuation tank which serve as a dump for the driver gas prior to entrance into the 16m long ram accelerator tube. The accelerator tube, which can be divided into sections separated by diaphragms, is filled with a pressurized fuel/oxidizer mixture and is instrumented at 40 axial locations. Instrumentation consists of pressure transducers, fiber-optic light guides, and magnetic transducers. Thin magnetic sheets are mounted in the nose-body joint and in the base of the projectile (see Figure 1). When the projectile passes electromagnetic transducers on the accelerator tube these magnets induce signals that are used to determine the distance-time history (i.e. velocity) of the projectile. Projectile thrust is derived from the velocity history. The ARL 120mm (bore diameter) facility is described by Kruczynski (1992).

The projectile consists of an axisymmetric cone-boattail body (blunt base) with stabilizing fins to center it along the launch tube axis (see Figure 1). The projectile is shaped like the centerbody of a ramjet engine and is injected into a stationary tube filled with a pressurized gas mixture of hydrocarbon fuel (e.g. CH_4), oxidizer and diluents such as CO_2 , N_2 , He, and Ar. There is no propellant on board the projectile. The tube resembles the outer cowl of a conventional ramjet engine. When the injection velocity is greater than the sound speed of the gas, a strong oblique shock system develops on the projectile which sustains combustion around the projectile. In this way the energy release process travels along with the projectile. Thrust is generated by the action of high pressure reacting gases on the

rear part of the projectile. Various combustion ignition mechanisms have been investigated including a perforated pusher sabot. The initial gas pressure, fuel/oxidizer composition, and sound speed can be selected to achieve the desired acceleration and projectile velocity at tube exit. Diluents are used to tailor the acoustic speed of the mixture so that the initial Mach number of the projectile exceeds the minimum required (≈ 2.8) to start the diffuser (i.e. projectile/tube clearance at maximum projectile body diameter) and tailors the heat release of combustion to a level that stabilizes the shock system on the projectile body. Excessive diluent results in low projectile acceleration levels, whereas insufficient diluent concentration can cause pre-ignition on the projectile forebody and deceleration. In addition, fuel lean mixtures can result in ignition on the projectile forebody.

The total force on the projectile is composed of the drag force on the forebody and a thrust produced by the high pressure combustion products on the projectile afterbody and base. Normally a net thrust is obtained since the pressure of the combustion products is higher than that of the compressed gases downstream of the nose shock. Gas mixtures with higher heat of reaction yield greater net thrust. Significant combustion must occur only on the afterbody of the projectile in order to maximize thrust since combustion on the conical nose contributes to the drag force. As the combustion moves farther behind the cone-boattail junction on the projectile (throat), smaller fractions of the afterbody surface area are exposed to high pressure gases resulting in reduced thrust.

Several modes of ram accelerator propulsion have been investigated experimentally (Bruckner 1988). The first mode applies to projectile operating velocities below the Chapman-Jouguet (CJ) detonation speed of the propellant mixture (Hertzberg 1988) which typically ranges in Mach number from 2.5 to 4 for hydrocarbon fuels. In this mode, the thrust is provided by the high pressure projectile base pressure resulting from a normal shock system stabilized on the body by theorized thermal choking of the reacting flow at full tube area behind the projectile (see Figure 2). One theoretical model of the thermally choked mode predicts that the normal shock recedes along the body as the projectile velocity increases (Bruckner 1988). If the projectile afterbody were to taper to a point and the flow were inviscid, this normal shock would gradually fall back to the full tube area. A normal shock in a constant area duct, followed by heat addition and thermal choking in steady flow, constitutes a CJ detonation wave. Thus, theory predicts that the thrust goes to zero as the projectile velocity approaches the CJ detonation speed of a particular propellant mixture (Bruckner 1988). For projectile speeds as high as 85% of the CJ detonation speed of the mixture, UW has observed that the thrust as a function of Mach number is indeed accurately predicted by the one-dimensional theoretical model of thermally choked mode (Bruckner 1988). At projectile velocities above 85% of the CJ detonation speed, however, the thrust typically

begins to exceed that predicted by the theoretical model, reaching a minimum at velocities near 95% of the CJ detonation speed of the mixture, and then tends to increase with velocity. This trend coincides with the experimentally observed combustion occurring on the projectile body. Combustion on the surface of the projectile, as opposed to solely in the projectile's wake was proposed by the present author based on numerical simulations (Nusca 1991). Experiments have shown that in this second mode called "transdetonative" (typically Mach number 4 to 6), the projectile can accelerate smoothly at or slightly above the CJ detonation speed of the mixture. For operating at higher Mach numbers, a "superdetonative" mode has been investigated (Bruckner 1988). This mode operates at velocities greater than the CJ detonation speed of the mixture. UW has proposed that this supersonic combustion process involves shock-induced combustion, wherein the mixture is ignited by one of several reflected oblique shock waves on the body. The supersonic heat release raises the gas pressure on the afterbody of the projectile, resulting in thrust as reacted propellant expands back to full tube area.

Typically, beyond the superdetonative mode, measured projectile thrust rapidly decreases perhaps due to extensive combustion on the forebody of the projectile. Each of the propulsion modes described above and observed in experiments at the UW has also been observed in numerical simulations (Nusca 1990,1991,1992).

3. NON-REACTING FLOW SIMULATION

The Reynolds-Averaged Navier-Stokes (RANS) equations for 2D/axisymmetric flow are written in the following conservation form. The dependent variables u , v , and e are mass-averaged.

$$\frac{\partial W}{\partial t} + \frac{\partial F}{\partial x} + \frac{\partial G}{\partial y} + \left(\frac{G}{y} - \frac{H}{y} \right) \alpha = 0 \quad (1)$$

$$W = \begin{pmatrix} \rho \\ \rho u \\ \rho v \\ \rho e \end{pmatrix}, F = \begin{pmatrix} \rho u \\ \rho u^2 - \sigma_{xx} \\ \rho uv - \tau_{xr} \\ \rho ue + \dot{q}_x - \sigma_{xx}u - \tau_{xr}v \end{pmatrix}, G = \begin{pmatrix} \rho v \\ \rho uv - \tau_{xr} \\ \rho v^2 - \sigma_{rr} \\ \rho ve + \dot{q}_r - \tau_{xr}u - \sigma_{rr}v \end{pmatrix},$$

$$H = \begin{pmatrix} 0 \\ 0 \\ -\sigma_+ \\ 0 \end{pmatrix}$$

where $\alpha = 1$ for axisymmetric flow and 0 for two-dimensional flow. Normal stresses (σ), shear

stress (τ_{xr}), heat transfer (\dot{q}), and internal energy (e) are defined in Nusca (Nov. 1991). The flow medium is assumed to be a perfect gas satisfying the equation of state,

$$p = \rho \Re T \quad (2)$$

The following power law was used to relate molecular viscosity to temperature (Mazor 1985):

$$\frac{\mu}{\mu_o} = \left(\frac{T}{T_o} \right)^n \quad (3)$$

where $\mu_o = 0.1716$ MPa, $T_o = 491.6$ R, and $n = 0.64874$. The laminar and turbulent Prandtl numbers, Pr and Pr_t , were assumed constant with values of 0.72 and 0.9 respectively. The ratio of specific heats, γ , was also assumed constant. The specific heat capacities at constant volume and pressure, c_v and c_p , are related as $\gamma = c_p/c_v$ and $\Re = (\gamma - 1)c_p/\gamma$.

Assuming a time-invariant grid and using the transformation of coordinates implied by $\tau = t, \xi = \xi(x, y), \eta = \eta(x, y)$, Equation 1 can be recast into conservation form where ξ and η are the new independent variables and x_ξ, x_η, y_ξ , and y_η are the four transformation coefficients obtained numerically from the mapping procedure (Chakravarthy 1985).

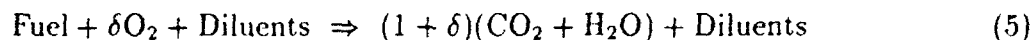
$$\frac{\partial W}{\partial \tau} + \frac{1}{\text{Area}} [(y_\eta F - x_\eta G)_\xi + (-y_\xi F + x_\xi G)_\eta + G/y - H/y] = 0 \quad (4)$$

The "Area" in Equation 4 denotes the area of the finite volume cell under consideration at the time of discretization of the equations.

The shock/boundary-layer interference flowfield between projectile and launch tube as well as the projectile wake can include regions of recirculating flow. Modeling of these regions can be critical to the overall flowfield solution quality. However, most existing turbulence models either do not treat such regions or do so in a semi-empirical fashion that is frequently inadequate. To improve the predictive capability of separated flows using RANS codes a new turbulence model has been developed (Goldberg 1986). The model is based on experimental observations of detached flows. The model prescribes turbulence kinetic energy (k) and dissipation (ϵ) analytically within backflows. A formula for the eddy viscosity (μ_t) distribution within backflows is derived and used for the RANS equations when the calculations are done inside separation bubbles. Outside of them, another turbulence model (Baldwin-Lomax, 1978) supplies the values of eddy viscosity. While the Baldwin-Lomax turbulence model is used to detect flow separation and to initiate application of the backflow model, the latter model can relocate the separation point.

4. REACTING FLOW SIMULATIONS

4.1 Chemical Reactions. Systems of chemical reactions are usually complex. A hydrocarbon fuel, for example, may contain hundreds of distinct chemical species. During combustion, numerous short-lived intermediate species are formed in addition to the final products that include H_2O and CO_2 . Any increase in computational accuracy by including all intermediate species and reaction steps within the framework of a calculation could be defeated by uncertainties in the thermodynamic, transport, and chemical-kinetic properties of these species. In addition, the computational costs of a given reaction mechanism depend primarily on the number of chemical species included, rather than on the number of reactions (Westbrook 1981). It is possible to make useful predictions of combustion processes by confining attention to a postulated global reaction between hydrocarbon fuel and oxidizer that neglects intermediate steps (Westbrook 1981).



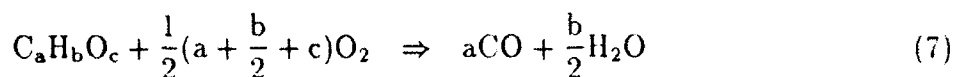
where δ is the stoichiometric oxidizer/fuel ratio. Several limitations of a global reaction model should be noted (Rogers 1983). During the ignition delay period, when the complete reaction mechanism will predict the gradual buildup of free radicals with little or no perceptible temperature change, a global model will indicate an immediate exothermic (or endothermic) reaction with resulting temperature increase (or decrease). Secondly, the adiabatic flame temperature predicted by the global model will be higher than for the complete multi-step reaction mechanism. This results from the fact that a global model does not include all the product species actually present in the reaction. If very low pressures are avoided, the discrepancy in flame temperature will not be significant (Rogers 1983). This overestimate of the adiabatic flame temperature increases with larger equivalence ratio (fuel/oxidizer) and is directly related to the amounts of CO and H_2 in the reaction products (Westbrook 1981). In addition, flame speed tends to decrease with increasing pressure for most hydrocarbon-air mixtures; thus, it may not be possible to reproduce both high and low pressure ranges with a single reaction rate expression (Westbrook 1981).

Hydrocarbon reactions are commonly used for ram accelerator testing at the University of Washington (Bruckner 1988) for example.



The fuel equivalence ratio, Φ , is a measure of the amount of fuel available for combustion. When $\Phi = 1$, the proportions of fuel to oxygen are stoichiometric. For Φ values smaller than unity fuel should be completely consumed. For the reaction stated above $\Phi = 2.7$ which is considered slightly outside the range of well understood CH_4/O_2 chemical kinetics

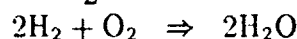
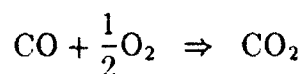
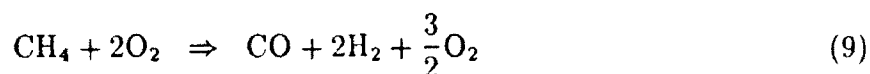
(Anderson 1991). This reaction is one of a general class of hydrocarbon reactions investigated by Westbrook and Dryer (1984),



where elemental and diluent species N_2 , C_2 , and H_2 are ignored thus ($a=1$, $b=4$, $c=1$),



CH_4 is considered the fuel, O_2 the oxidizer, and products are CO_2 and H_2O . A three-step reaction mechanism has also been proposed by Westbrook (1991) in which CH_4 is oxidized to CO and H_2 with subsequent oxidation of CO and H_2 forming CO_2 and H_2O .



4.2 Reaction Rates and Kinetics. Conservation of chemical species can be written for each specie in Equations 8 and 9. Because a rate term is included the governing equations are mathematically stiff. Stiffness can be defined as the ratio of the largest to the smallest time scale. In reacting flows, time scales associated with chemistry tend to be much smaller than time scales of the fluid motion, sometimes by orders of magnitude. In the present code the stiffness problem is resolved by uncoupling the fluid dynamics equations from the species conservation (rate) equations for a fixed number of numerical iterations (or sub-iterations between time steps), then updating the rate terms. The reaction rate is defined (Westbrook 1981, 1984) using the Law of Mass Action and an Arrhenius expression for C , the specific reaction rate constant.

$$R = C \prod_1^N m_j^{n_j} = \bar{A} T^\alpha \exp\left(\frac{-E_a}{\bar{R}T}\right) m_{CH_4}^a m_{O_2}^b m_{CO}^c m_{H_2}^d \quad (10)$$

where and $N = 4$ (for Eq. 8), $\bar{A}T^\alpha$ is the collision frequency, the exponential term is the Boltzmann factor, and E_a is the activation energy. The reactant mass fraction terms ($m_{CH_4}^a, m_{O_2}^b$) for the 1-step reaction mechanism (Eq. 8) are raised to non-stoichiometric coefficients in order to simulate the rate limiting step ($CO + \frac{1}{2}O_2 \Rightarrow CO_2$) of the 3-step mechanism (Eq. 9). For reaction sets given by Equations 8 and 9, Westbrook (1977, 1981, 1984) specifies \bar{A} , E_a , a, b, c and d with $\alpha = 0$ and $\bar{R} = 8.314$ J/K-mole (see Table 1).

Westbrook and Dryer (1981) used a simple procedure for obtaining the single-step reaction rate expression (Eq. 10). Values for the concentration exponents a and b were held fixed

Table 1. Reaction Rate Equation Data

Reaction	E_a (kcal/mole)	\bar{A} (moles/cm ³ -s)	a	b	c	d
Eq. 8	30.0	8.3×10^5	-0.3	1.3	0.0	0.0
Eq. 9, step 1	30.0	8.3×10^5	1.0	2.0	0.0	0.0
Eq. 9, step 2	44.7	3.0×10^6	0.0	0.5	1.0	0.0
Eq. 9, step 3	37.6	1.0×10^5	0.0	1.0	0.0	2.0

at the values stated above. They found that the relation $a + b = 1$ was necessary in order to properly reproduce the correct dependence of flame speed on pressure for gas mixtures where Φ is not unity. As expected the flame speed depends strongly on a for fuel-rich mixtures. For $a = -0.3$ the fuel acts as an inhibitor which matches observations for methane ignition in shock tubes. The activation energy, E_a , was also held fixed and the pre-exponential factor \bar{A} was varied until the model correctly predicted measured flame speed for atmospheric pressure and $\Phi = 1$. The resulting rate expression was then used to predict flame speed for other values of pressure and Φ . Each set of rate expression parameters was evaluated on the basis of how well it reproduced experimental data (flame speed). The results showed that varying E_a from 26-50 kcal/mole (for Eq. 8) effected the flame thickness alone. Westbrook (1981) suggests $E_a = 30$ and 48.4 kcal/mole as the most appropriate values.

4.3 Governing Equations. The conservation equations for mass (global) and momentum are the same as those given in Equation 1. Additionally, for reacting flows, species mass conservation is given by,

$$\frac{1}{r} \left[\frac{\partial}{\partial r} (r \rho u m_j + r J_{j,r}) + \frac{\partial}{\partial z} (r \rho w m_j + r J_{j,z}) \right] - R_j = 0 \quad (11)$$

where R_j is the reaction rate per unit volume for species j . Energy conservation for a compressible reacting, flow is expressed by the same energy equation as used for non-reacting flow (see Eq. 1) if expressed in terms of the total enthalpy (\tilde{h}),

$$\nabla \cdot \left[\rho \tilde{V} \tilde{h} + \tilde{J}_h + \sum_j h_j \tilde{J}_j + \tilde{J}_k - (u \tilde{\tau}_r + v \tilde{\tau}_\theta + w \tilde{\tau}_z) \right] = 0 \quad (12)$$

where \tilde{J} is a flux term for mass ($\tilde{J}_j = (\mu_{eff}/Re) \nabla m_j$), heat ($\tilde{J}_h = (\mu_{eff}/Pr) c_p \nabla T$), and turbulence kinetic energy ($\tilde{J}_k = (\mu_{eff}/Pr) \nabla k$). The mass fraction and molar specific enthalpy for species j are m_j and h_j , respectively. Radiation flux is neglected in Equation 12.

In Equation 12 the shear stress ($\tilde{\tau}$) includes the Reynolds stress with an effective fluid viscosity expressed as the sum of the molecular and turbulent viscosities, $\mu_{eff} = \mu + \mu_t$.

A Wilke's mixing law is used to compute the chemically reacting mixture viscosity. The calorically perfect gas assumption can be made when the temperature dependence of c_p , for the reactants and products is not well determined. The specific heat can also be formulated using an explicit temperature dependence obtained from tabulated data (Stull 1971).

$$c_p/\bar{\mathcal{R}} = A_1 + A_2T + A_3T^2 + A_4T^3 + A_5T^4 \quad (13)$$

For N species only $N - 1$ specie equations must be solved, since the sum of the mass fractions must equal unity. In effect the global continuity equation is the N th specie equation since the summation of all specie equations yields the continuity equation. The mixture equation of state for a thermally perfect gas follows from Dalton's Law,

$$p = \rho \bar{\mathcal{R}} T \sum_j^N \frac{m_j}{\mathcal{M}_j} \quad (14)$$

where $\bar{\mathcal{R}} = \mathcal{R} \sum_j \mathcal{M}_j$, \mathcal{M}_j is the molecular weight of species j , and \mathcal{R} is the specific gas constant. Mixture temperature (T) is obtained from the definition of the stagnation enthalpy,

$$\tilde{h} = T \sum_j^N c_{p,j} m_j + \left[1 - \frac{1}{\text{Pr}}\right] \frac{V^2}{2} + \left[\frac{1}{\text{Sc}} - \frac{1}{\text{Pr}}\right] \frac{\hat{V}^2}{2} + \left[\frac{1}{\text{Sc}} - \frac{1}{\text{Pr}}\right] \sum_j h_j m_j \quad (15)$$

with $V = (u^2 + v^2 + w^2)^{1/2}$, and \hat{V} is the magnitude of the turbulent (fluctuating) velocity. The Schmidt number (Sc) is assumed to be unity. The Prandtl number (Pr) is assumed to be nearly unity (.9) which is considered adequate for gaseous flows even with combustion (Bradshaw 1981). Mixture viscosity (μ) is defined using Sutherland's expression (Ames Research Staff 1958) for $T \leq 3400\text{R}$ and using Equation 3 for higher temperatures.

A two-equation turbulence model has been suggested by Kim and Chung (1989) for reacting flows. This model describes the turbulence viscosity (μ_t) as a function of turbulence kinetic energy (k) and dissipation rate (ϵ) as $\mu_t = \rho C_3 k^2 / \epsilon$. A set of partial differential equations is written for k and ϵ .

$$\rho w \frac{\partial k}{\partial z} + \rho u \frac{\partial k}{\partial r} - \frac{1}{r} \left[\frac{\partial}{\partial z} \left(r \mu_k \frac{\partial k}{\partial z} \right) + \frac{\partial}{\partial r} \left(r \mu_k \frac{\partial k}{\partial r} \right) \right] = G - \rho \epsilon \quad (16)$$

$$\rho w \frac{\partial \epsilon}{\partial z} + \rho u \frac{\partial \epsilon}{\partial r} - \frac{1}{r} \left[\frac{\partial}{\partial z} \left(r \mu_\epsilon \frac{\partial \epsilon}{\partial z} \right) + \frac{\partial}{\partial r} \left(r \mu_\epsilon \frac{\partial \epsilon}{\partial r} \right) \right] = B \quad (17)$$

$$B = \frac{C_1 G \epsilon}{k} - \frac{C_2 \rho \epsilon^2}{k} \quad (18)$$

$$\frac{G}{\mu_t} = 2 \left(\left(\frac{\partial w}{\partial z} \right)^2 + \left(\frac{\partial u}{\partial r} \right)^2 + \left(\frac{u}{r} \right)^2 \right) + \left(\frac{\partial w}{\partial r} + \frac{\partial u}{\partial z} \right)^2 \quad (19)$$

where, $\mu_k = \mu + \mu_t/\lambda_k$, $\mu_\epsilon = \mu + \mu_t/\lambda_\epsilon$, $\lambda_k = 1$, $\lambda_\epsilon = 1.3$, $C_1 = 1.44$, $C_2 = 1.92$, $C_3 = .09$. These equations are solved along with the Navier-Stokes equations. Boundary conditions for k and ϵ are $k = 0$, $\epsilon = .056\mu(\partial u/\partial y)^2/\rho$ for solid walls and $k = 10^{-6}V_\infty^2$, $\epsilon = k^{1.5}/L$ for freestream. Initial conditions are $k = k_\infty$, $\epsilon = k^{1.5}C_3^{-0.5}/(.37x^{0.8}Re^{-0.4})$.

5. NUMERICAL ALGORITHMS

The spatial discretization technique for the equations of motion must be reliable and robust if it is to successfully capture the complex physics of in-bore projectile/launch tube interacting flowfields. The TVD formulation for the convective terms along with a special treatment of the dissipative terms provides an appropriate simulation. In recent years, TVD formulations have been constructed for shock-capturing finite-difference methods (Chakravarthy 1985). Near large gradients in the solution (extrema) TVD schemes automatically reduce to first-order accurate discretizations locally while away from extrema they can be constructed to be of higher-order accuracy. This local effect restricts the maximum global accuracy possible for TVD schemes to third order for steady-state solutions. TVD methods manifest many properties desirable in numerical solution procedures. By design they avoid numerical oscillations and "expansion shocks" while at the same time being of higher-order accuracy. TVD formulations are also based on the principle of discrete or numerical conservation which is the numerical analog of physical conservation of mass, momentum, and energy. Thus, TVD schemes can "capture" flowfield discontinuities (e.g. shock waves) with high resolution. At a fundamental level they are based on upwind schemes; therefore, they closely simulate the signal propagation properties of hyperbolic equations. Schemes based on the TVD formulation are completely defined. In contrast, schemes based solely on central differences involve global dissipation terms for stability and have one or more coefficients that must be judiciously chosen to achieve desirable results. Any conventional time discretization method suitable for the Navier-Stokes equations can be used together with this space discretization methodology; for example, approximate factorization and relaxation techniques.

5.1 Flowfield Grids. Computing in-bore projectile flowfields is complicated by the multi-wall geometry. The ram accelerator projectile consists of several sharp corners that would severely hamper conventional grid generation schemes that require one set of grid lines to be tangent to surfaces and another set to be normal to them. This geometry is more easily gridded by the zonal approach. The internal geometry of the ram accelerator launch system is broken up into three zones of simple geometric shape (zone 1 between the projectile and the launch tube, zone 2 in the projectile wake and zone 3 aft of the obturator).

An algebraic grid is generated in each zone with clustering near surfaces and other regions in the flowfield where high gradients are expected. The zonal boundaries are transparent to flowfield phenomena (e.g. shock waves). The actual grid used for these computations ($\approx 56,000$ nodes) consisted of the following dimensions for zones 1 and 2/3: 261x41, 741x61. The computational domain starts a small distance forward of the body and extends 4.5 projectile body lengths downstream. The computational results were found to be essentially independent of further grid refinement when all other factors were the same. A dense grid is preferred for resolving flow details within boundary layers, to prevent shock smearing, and to resolve shock/boundary-layer interactions.

6. RAM ACCELERATOR CONFIGURATIONS

For the simulation of projectile/obturator separation, the University of Washington 38mm system shot CS10 (N_2 gas fill) was used (Knowlen 1992). The projectile consisted of a 12.5-degree, 65mm long conical forebody and 6.25-degree, 50.8mm long conical afterbody. The projectile base diameter was 17.8mm. The obturator was 14.2mm thick (12 grams) and consisted of 5mm diameter holes, 19 in number or approximately 33% porous. For the reacting flow simulations, the projectile consisted of a 10-degree, 83mm conical forebody and 8-degree, 71mm conical afterbody. The obturator was 16mm thick and consisted of 5mm diameter holes, 19 in number or approximately 33% porous. For comparison to the ARL 120mm ram accelerator system these 38mm system configurations were not simply scaled but the actual 120mm system geometry was used. The projectile consisted of a 10-degree, 261mm conical forebody and 4-degree, 261mm conical afterbody. The obturator was 112mm thick (1.1915 kg) and was assumed to be of the same porosity as the 38mm system. In all configurations the projectile fins were ignored as well as the non-porous obturator backplate.

7. RESULTS

Simulation of the projectile/obturator separation (ignoring the separation of the solid obturator backplate) was accomplished by assuming that the projectile and obturator were mated as they entered the accelerator tube from the launch tube. Simulation of the launch tube section of the system is addressed by Nusca (Oct. 1992). The velocity of the projectile as it traversed the accelerator tube was measured for the University of Washington's shot CS10 and was specified in the simulation. Separation of the obturator due to the aerodynamic forces acting on both sides of the disk was simulated by computing a obturator force coefficient as the time-accurate simulation was run. This coefficient along with the

obturator mass was used to update the obturator position (and re-grid zones 2 and 3 of the computational domain) with respect to the projectile, during the run. The simulation was stopped periodically (corresponding to the location of measurement stations on the University of Washington's system) to examine the accelerator tube wall pressure and compare to measured data. The results included in this report focus on the first two stations (i.e. up to .751m from the entrance) although the simulation was run for 3.0m along the accelerator tube (6m in length). For CS10 the tube was filled with nitrogen gas at 35 atm. The entrance velocity of the projectile/obturator was taken as 1335 m/s (from measurements). The 120mm system used for comparison has a fill pressure of 68 atm and entrance velocity of about 1200 m/s. The numerical simulation was performed from the fixed projectile reference frame with the accelerator tube moving at a fixed (or variable) velocity along with a slug of gas upstream of the projectile. As a result, the boundary layer on the accelerator tube wall does not form until the first shock reflection. The holes in the obturator were treated by assuming uniform porosity of 33%.

Figure 3 shows the projectile velocity versus distance along the accelerator tube as measured at the University of Washington (shot CS10) used for the simulations. The computed obturator velocity, initially the same as the projectile's rapidly decreased as measured but at values about 15% higher. For the 120mm system, the obturator velocity is about 10% lower indicating that it separates more slowly. This is not only due to the mass of the 120mm system obturator but the lower pressures on the obturator surface (relative to those in the 38mm system). Scaling of the fluid dynamics has therefore not been completely accomplished.

Figure 4 shows the computed obturator force coefficient as a function of separation from the projectile. Initially the force is high, but as the obturator separates from the projectile this force decreases (relief effect) and then increases with separation distance. The shielding of the obturator from the oncoming flow (relative to the projectile-based coordinate system) is gradually removed and the drag rises. The force on the obturator for the 120mm system, for the same relative separation distance, is slightly smaller initially and slightly greater at larger separation. This indicates a lower initial obturator surface pressure, as mentioned previously.

Figures 5 illustrates the flowfields over the projectile/obturator configurations at measurement stations 1 and 2 (as well as pre-station 1) in the 38mm system. These pressure contours highlight areas of large pressure gradients and show that the projectile base flow is effected by the presence of the obturator.

Figures 6 and 7 show the accelerator tube wall pressure as measured in the University of Washington's 38mm system and computed in the ARL simulation. Figure 6 shows station 1

(just after entrance to the accelerator tube) pressures where the obturator is computed to be located approximately 78mm (67% projectile length) behind the projectile base (note that the projectile is .116m long). Pressure rises over the projectile are indicative of nose-shock reflections from the tube wall. These pressures are smaller than measured due to the absence of the projectile fins in the simulation. The double pressure peaks in front of the obturator location are seen in the measured and computed data. As indicated previously the obturator is slightly aft of the measured location (higher velocity, see Figure 3) in the simulation. The smaller pressure computed behind the obturator location is due to the downstream boundary condition imposed (i.e. tube fill pressure as opposed to gas pressure with venting created by the launch/vent tube which was not part of the present simulation). Figure 7 shows results for station 2 where the obturator is computed to be approximately 240mm (200% projectile length). The overall pressure levels are lower and the agreement between measured and computed data is better. The measured pressure rise at about .25m in Figure 7 occurs at about .28m in the simulation. The back pressure mismatch is again due to the downstream pressure boundary condition.

Figures 8 and 9 compare the computed accelerator tube wall pressures for the 38mm and 120mm systems. Due to the different projectile lengths, the x-axis has been made nondimensional. The gas pressure in the 38mm system was 35 atm while the 120mm system was charged to 68 atm. Since the 120mm system projectile has a different forebody angle (see section "Ram Accelerator Configurations") the pressure spikes are larger and at slightly different locations for this system. The pressures in the vicinity of the obturator are slightly lower for the 120mm system at station 1 (Figure 8) but slightly higher at station 2 (Figure 9), which is consistent with the data in Figure 4. As the obturator separates more significantly from the projectile (Figure 9) trends in pressure levels (downstream of the projectile) are comparable for the two systems. This reflects the fact that some fluid dynamic analysis has been used in the design of the 120mm system projectile in order to achieve a good scaling match to the 38mm system.

Figure 10 shows the results from a projectile/obturator separation simulation for reacting flow, methane/oxygen/nitrogen mixture at 12 atm fill pressure in the 38mm system. The projectile/obturator geometry is slightly different (as detailed in the last section). In this figure the obturator is computed to be approximately 56mm (37% projectile length of 154mm) behind the projectile base. The computation is for finite-rate chemical kinetics (three-step global model). Computed pressures before the reaction zone (before about .12m in the figure) compare well with measured data. In the reaction zone pressures are slightly smaller (due to the simplified chemical kinetics model) for the computation. Pressures near the obturator location are similar to measurements with smaller back pressure since the launch

tube section has been ignored (see previous discussion). Figure 11 shows the projectile thrust in the 38mm system as a function of velocity. Overprediction of the thrust is expected to be corrected when more detailed chemistry models (i.e. more reaction steps) are included.

8. CONCLUSIONS AND FUTURE WORK

Computational fluid dynamics solutions of the Navier-Stokes equations have been applied to both non-reacting and reacting in-bore flowfields for a ram accelerator projectile launch system. Good comparison between computed and measured pressures for non-reacting flow in a 38mm system was achieved, including the investigation of geometric scaling to a 120mm system. Previous publications by the ARL have focused on the simulation of projectile flow phenomena in the accelerator. The present work represents numerical simulation of projectile/obturator separation and the starting mechanism after projectile/obturator entrance into the accelerator tube. Good agreement with measured pressures during obturator separation has been achieved. Application of more detailed reaction kinetic models, as well as the investigation of the launch/vent tube (pre-accelerator) sequence, is warranted.

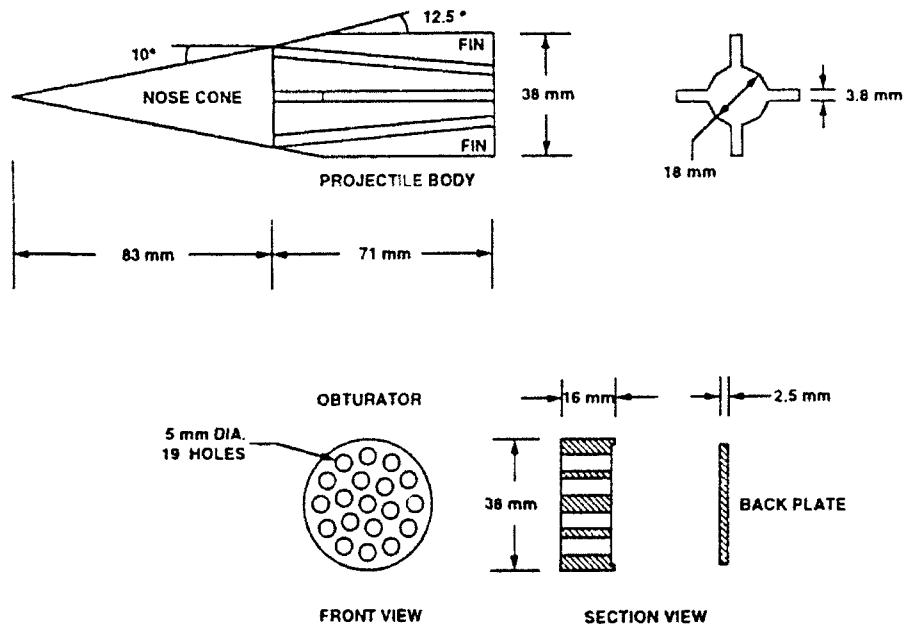


Figure 1. Schematic of projectile and obturator used in University of Washington experiments.

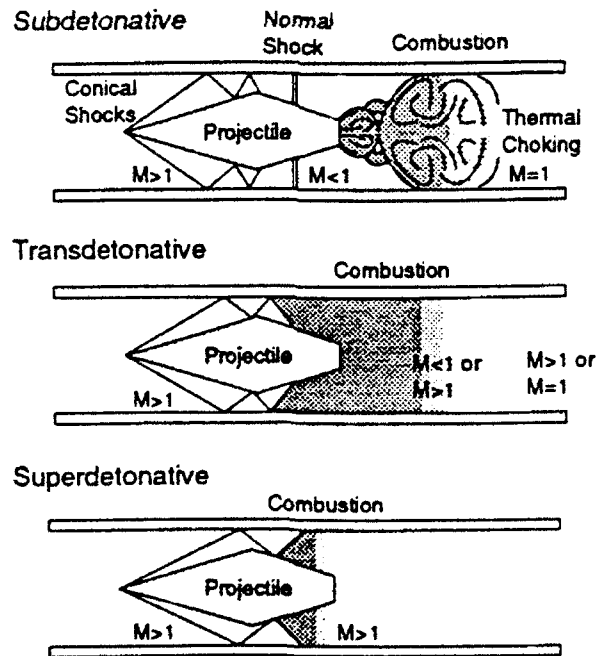


Figure 2. Schematics of thermally choked, transdetonative and superdetonative ram accelerator operating modes.

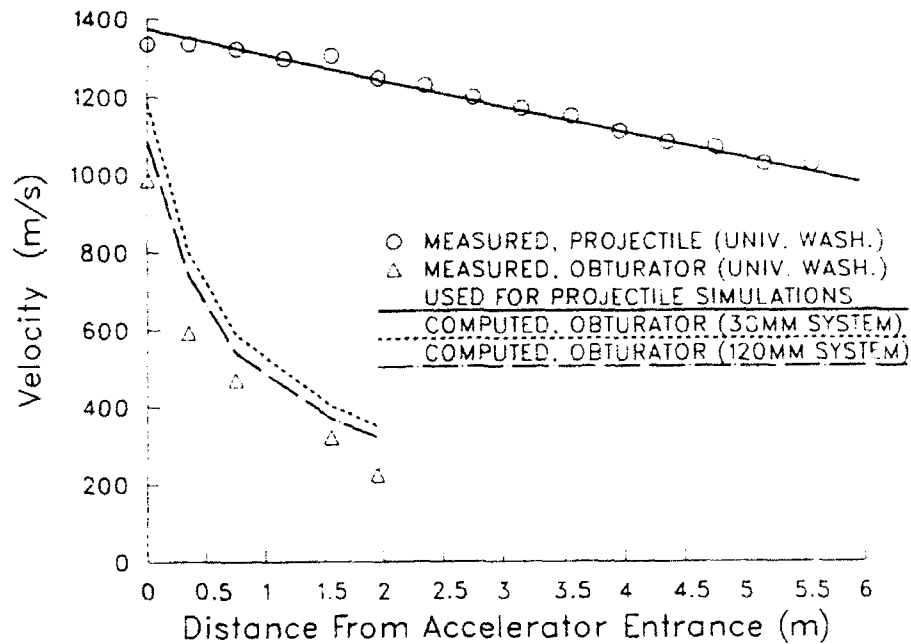


Figure 3. Projectile and obturator velocity along the accelerator tube, nitrogen gas fill (35 atm), 38mm and 120mm systems.

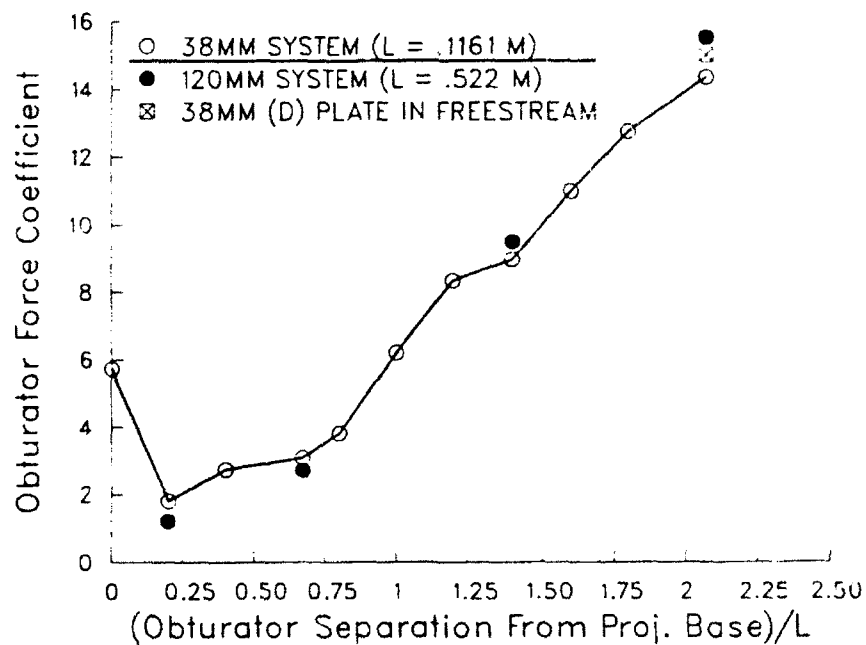


Figure 4. Computed obturator force coefficient (F/P_A) as obturator separates from projectile, nitrogen gas fill, 38mm (35 atm) and 120mm (68 atm) systems.

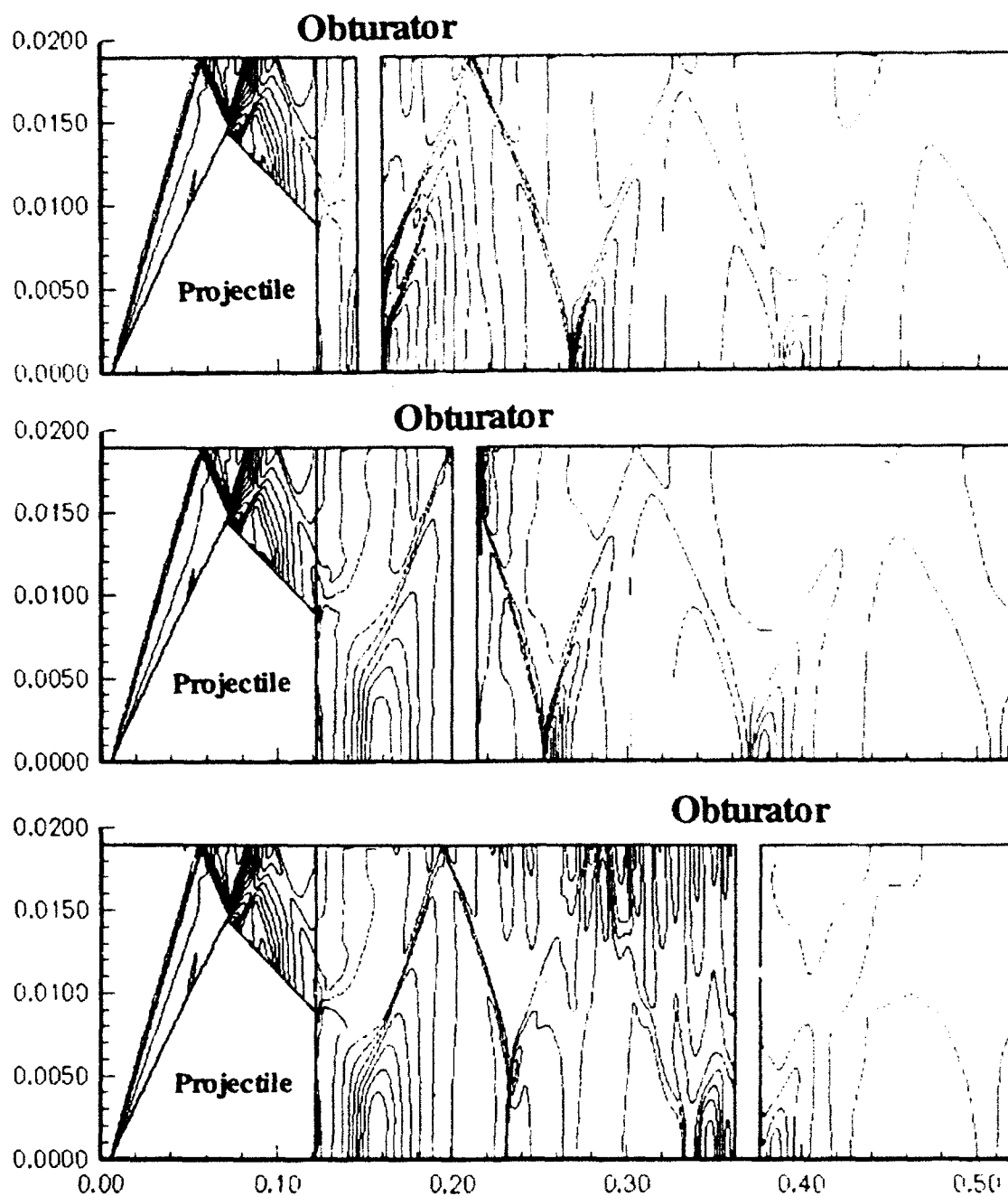


Figure 5. Computed pressure contours for nitrogen gas fill (35 atm), 38mm system, three stations in accelerator tube. Pre-first station with obturator at approx. 0.14 meters (computed), first station with obturator at approx. 0.2 meters (computed), second station with obturator at approx. 0.36 meters (computed). Axes are lengths in meters. Note magnified y-scale, i.e. angles on projectile are not true.

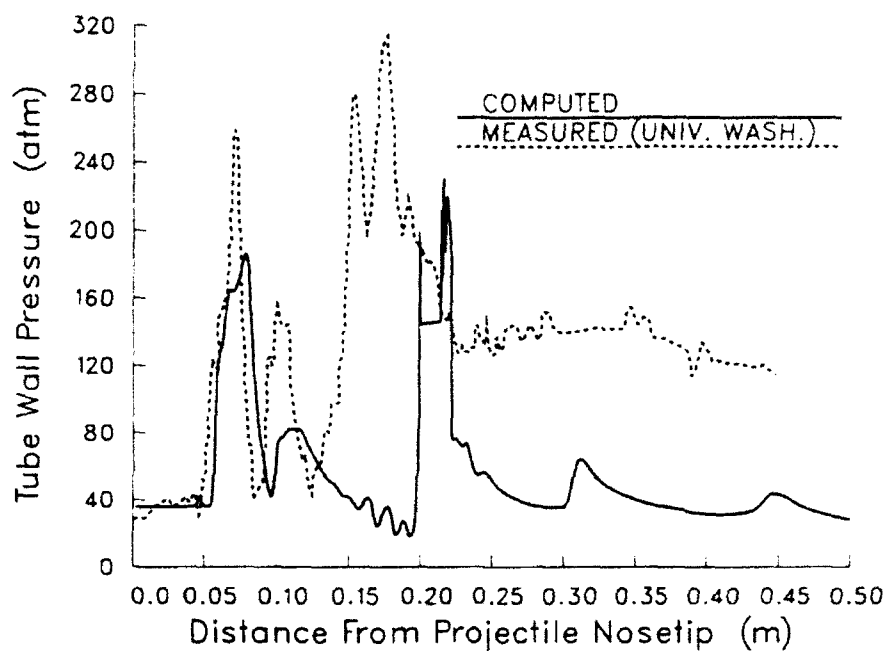


Figure 6. Tube wall pressure for nitrogen gas fill (35 atm), 38mm system, first station in accelerator tube, obturator at approx. 0.2 meters (computed).

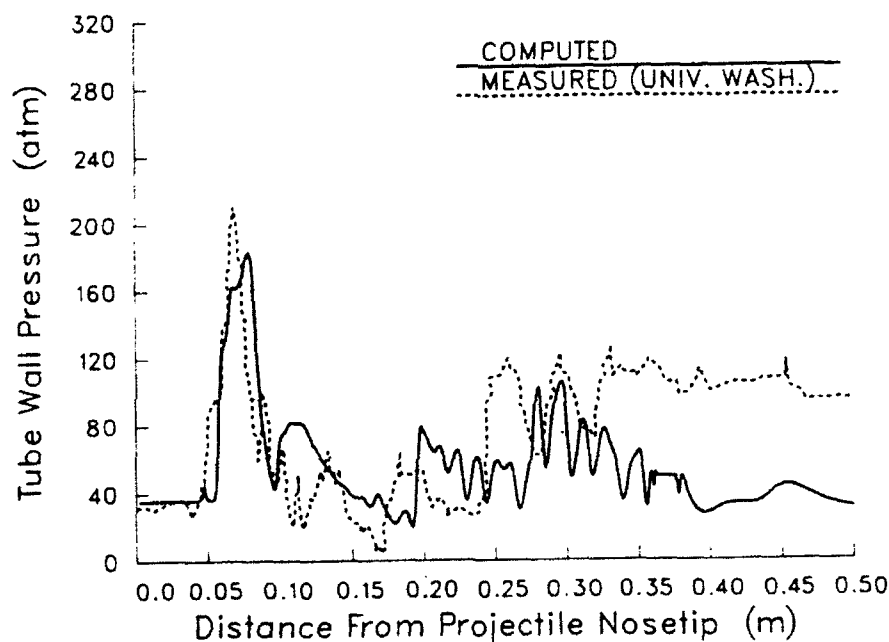


Figure 7. Tube wall pressure for nitrogen gas fill (35 atm), 38mm system, second station in accelerator tube, obturator at approx. 0.36 meters (computed).

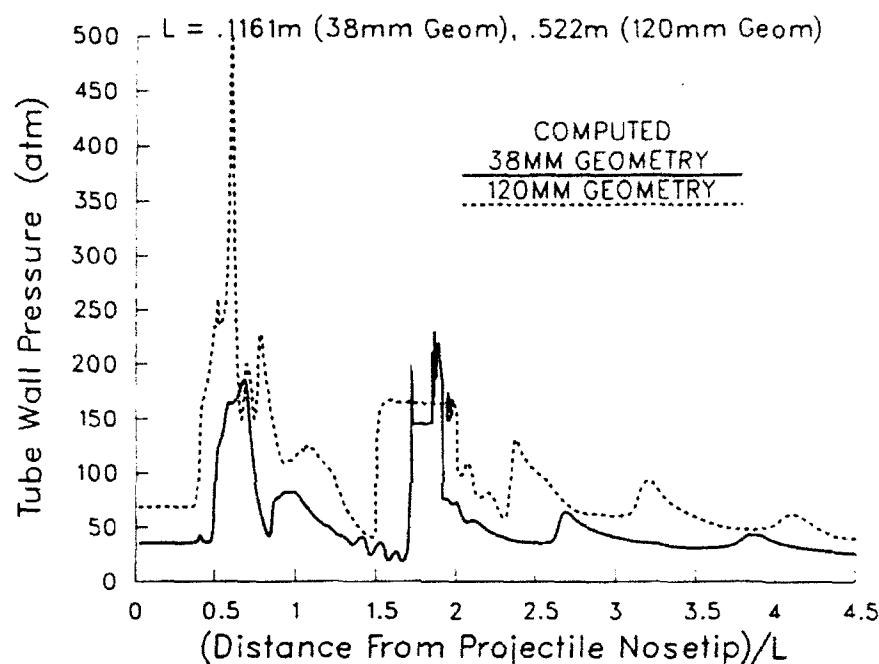


Figure 8. Computed tube wall pressure for nitrogen gas fill, 38mm (35 atm) and 120mm (68 atm) systems, first station in accelerator tube, obturator at approx. 1.7 L (computed).

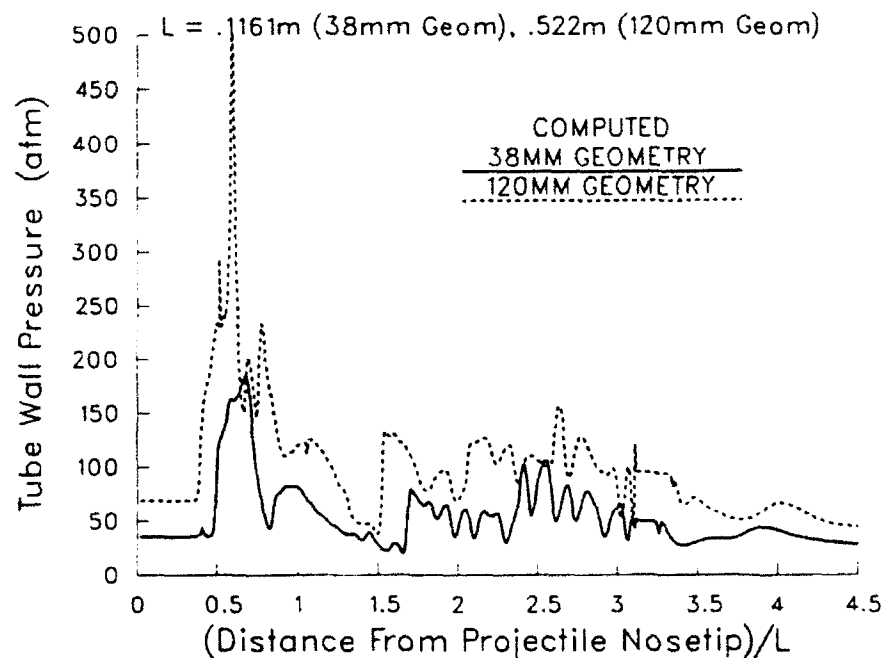


Figure 9. Computed tube wall pressure for nitrogen gas fill, 38mm (35 atm) and 120mm (68 atm) systems, second station in accelerator tube, obturator at approx. 3.1 L (computed).

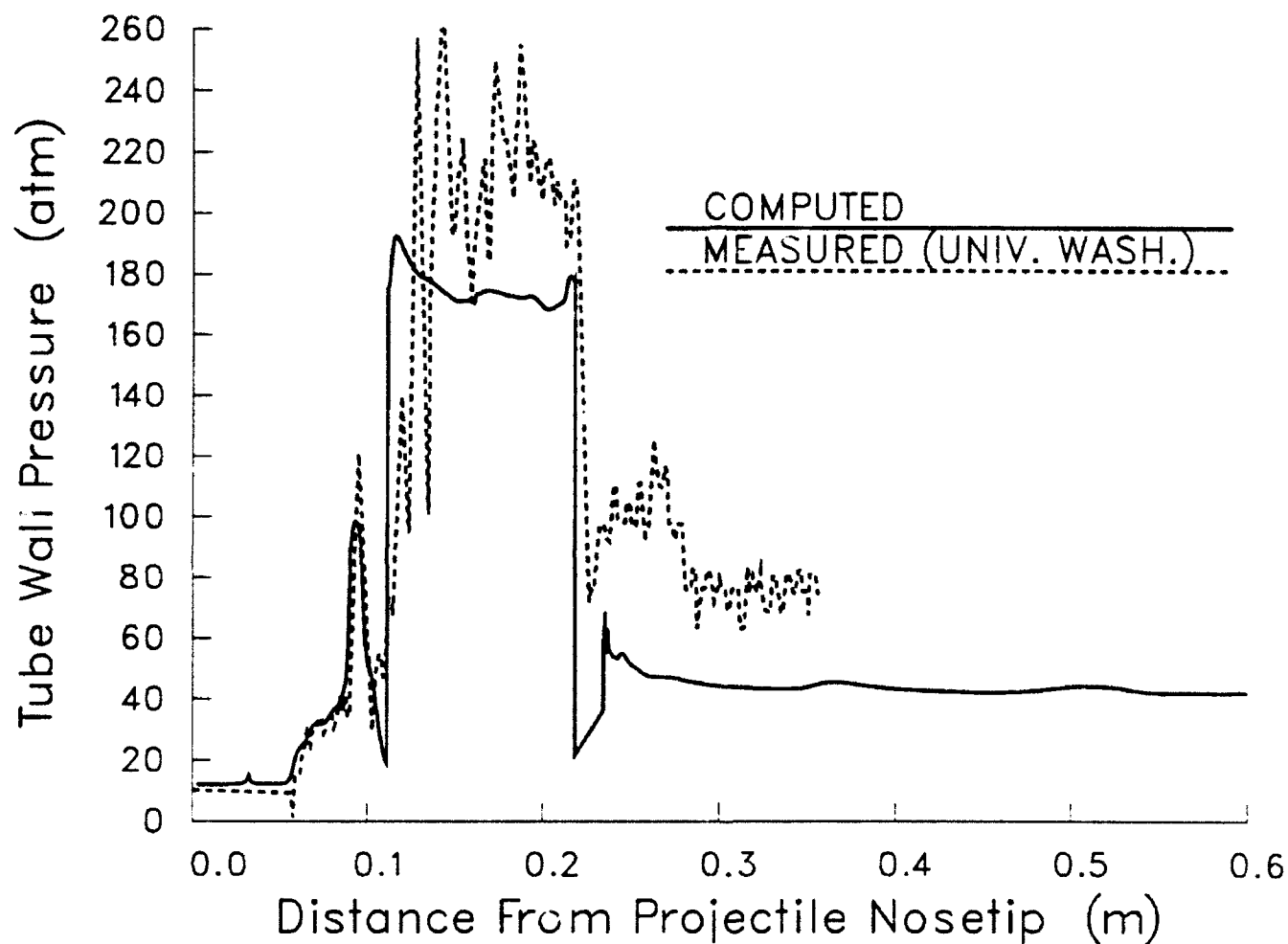


Figure 10. Tube wall pressure for reacting $2.7\text{CH}_4 + 2\text{O}_2 + 5.6\text{N}_2$ gas fill (12 atm), 38mm systems, first station in accelerator tube, obturator at approx. 0.22 m (measured).

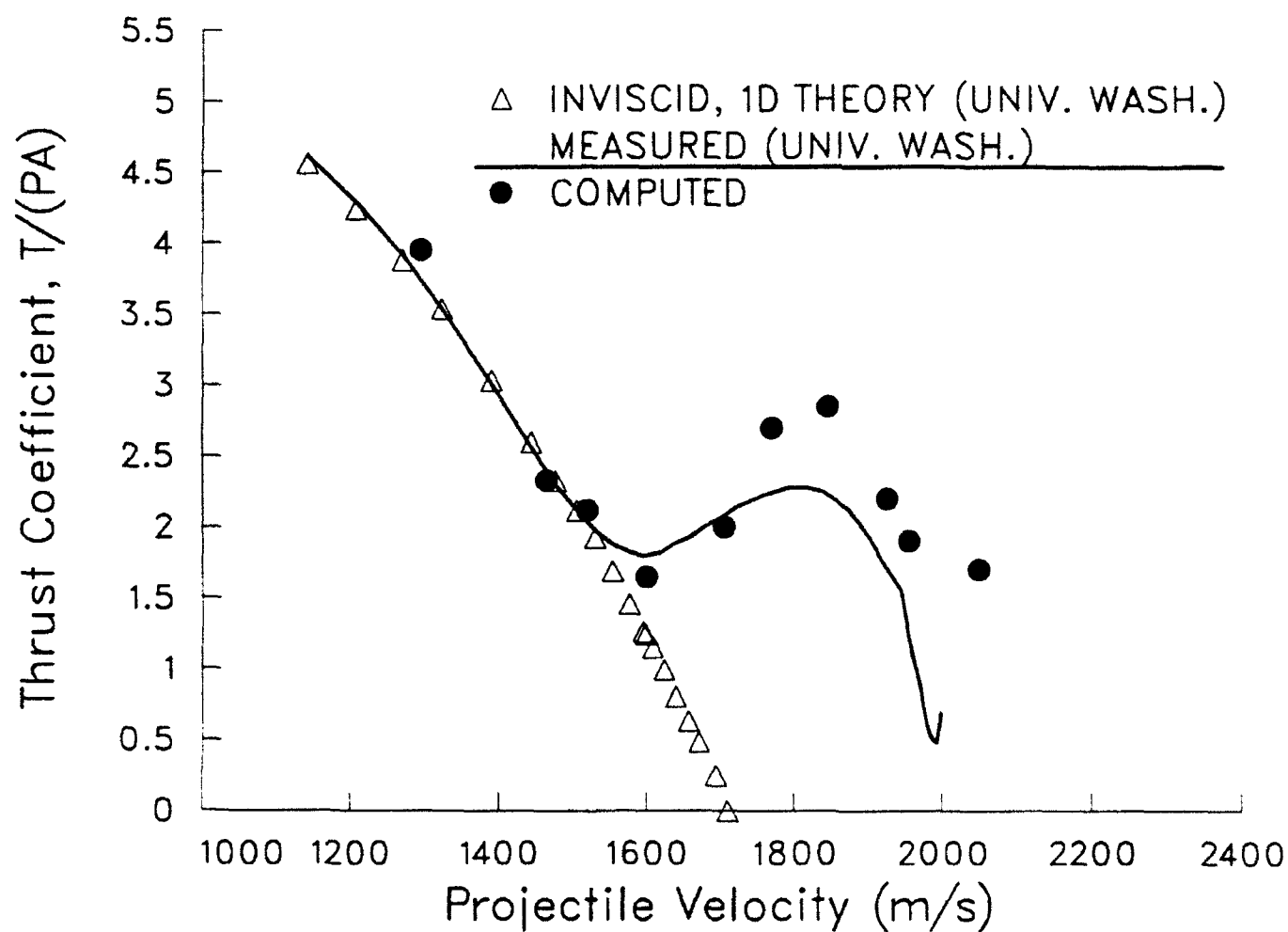


Figure 11. Projectile thrust coefficient vs. projectile velocity for reacting $2.7CH_4 + 2O_2 + 5.6N_2$ gas fill (20 atm), 38mm system ($A = .0011m^2$).

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LIST OF SYMBOLS

A	cross sectional area of launch tube
c_p	specific heat capacity, constant p
c_v	specific heat capacity, constant volume
C	specific reaction rate constant
e	specific total internal energy
E_a	activation energy
F, G, H	flux vectors (Eq. 1)
h	molar specific enthalpy
\tilde{h}	total enthalpy
J	flow rate or flux
k	turbulence kinetic energy
L	total body length
m	species mass fraction
\mathcal{M}	molecular weight
n	stoichiometric coefficient
N	number of species
p	static pressure
Pr	Prandtl Number, $\mu c_p / \kappa$
\dot{q}	heat transfer rate
r	radial direction
R	reaction rate per unit volume
\Re	specific gas constant, $(\gamma - 1)c_p/\gamma$
$\tilde{\Re}$	universal gas constant, $\Re \sum_j \mathcal{M}_j$
Re	Reynolds Number, $\rho V L / \mu$
Sc	Schmidt Number, μ / Γ
t	time
T	static temperature
\mathcal{T}	thrust

u	axial velocity
v	radial velocity
V	magnitude of the local velocity vector
W	dependent variable vector (Eq. 1)
x, y	cartesian coordinates

Greek Symbols

α	parameter (Eq. 1, 10)
γ	ratio of specific heats, c_p/c_v
Γ	diffusion coefficient
δ	stoichiometric oxidizer/fuel mass ratio
ϵ	turbulence dissipation rate
η	transformed coordinate
κ	heat transfer coefficient
μ	molecular viscosity
ξ	transformed coordinate
ρ	density
σ	normal stress
τ	transformed time
τ_{rr}	shear stress tensor
$\vec{\tau}$	shear stress vector
Φ	fuel equivalence ratio

Superscripts

$\hat{\cdot}$	unit vector
\cdot	total or stagnation
\cdot	rate

Subscripts

eff	effective
h	enthalpy
j	j -th mixture component or species
k	turbulence kinetic energy
p	constant pressure
r	radial component or radial direction
t	turbulence quantity
v	constant volume
x	x -direction
z	axial component
ϵ	turbulence dissipation rate
η	η -direction transform coefficient
θ	azimuthal component
ξ	ξ -direction transform coefficient
∞	freestream quantity

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